IVR: Characterisation of a Control System

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informatics

- Modelling an control system
- Stationary behaviour and time constant of control systems
- Model identification

Differential Equations

$$\frac{dx(t)}{dt} = f(x(t)) \text{ subject to } x(t_0) = x_0$$

• Example from last lecture:

$$rac{dx(t)}{dt} = ax(t)$$
 subject to $x(t_0) = x_0$

Solution

$$x(t) = x_0 \exp\left(a(t-t_0)\right)$$

- a > 0 fast increase for $x_0 > 0$
- a < 0 decay with time constant $\tau := -\frac{1}{a}$

Example: Electric motor

• Ohm's law & Kirchhoff's law

$$V_B = IR + e$$

- Motor generates voltage $e = k_1 s$
- Vehicle acceleration

$$\frac{ds}{dt} = \frac{\tau}{M}$$



$$\tau = k_2 I$$

• Putting together:

$$V_B = \frac{M}{k_2} R \frac{ds}{dt} + k_1 s$$







Solving differential equations numerically

Given process model

$$V_B = k_1 s + \frac{M}{k_2} R \frac{ds}{dt}$$

Rewrite

$$rac{ds}{dt} = -rac{k_1k_2}{RM}s + rac{k_2}{RM}V_B$$

2 Choose a small step size Δt

$${f S}$$
 Start at $t=0$ and $s(0)=s_0$

- Iterate $s(t + \Delta t) = s(t) + \Delta t \frac{ds}{dt}$ until t = T
- Solution How do control s(t) towards a desired value by changing V_B ?

Abstract form as a control system

 $C = As + B\frac{ds}{dt}$ $A + B\frac{d}{dt}$ sC

control system process dynamics state variable control variable plant and controller operator applied to state output: plant \rightarrow controller input: controller \rightarrow plant



Back to the Example

$$V_B = k_1 s + \frac{M}{k_2} R \frac{ds}{dt}$$

 $C = As + B\frac{ds}{dt}$ with $A = k_1$, $B = \frac{M}{k_2}R$, $C = V_B$ Stationary behaviour $s(t \to \infty) = \frac{C}{A}$

$$rac{ds}{dt}=0 \implies V_B=k_1s \implies s\left(t
ightarrow\infty
ight)=rac{V_B}{k_1}$$

Time scale (decay by a factor of $\frac{1}{e}$)

$$\tau = \frac{B}{A} = \frac{MR}{k_1k_2}$$

Half-life of decay

Decay by a factor of $\frac{1}{2}$

$$s(t) = s_0 e^{-\frac{k_1 k_2}{MR}(t-t_0)} + \frac{V_B}{k_1} \left(1 - e^{-\frac{k_1 k_2}{MR}(t-t_0)}\right)$$

Starting from previous state $s_0 = 0$ towards new stationary behaviour at $s = \frac{V_B}{k_1}$



$$\begin{pmatrix} \frac{1}{2} \end{pmatrix} \frac{V_B}{k_1} = \frac{V_B}{k_1} \left(1 - e^{-\frac{k_1 k_2}{MR}(t - t_0)} \right)$$
$$\frac{1}{2} = e^{-\frac{k_1 k_2}{MR}(t - t_0)}$$
$$t_{\text{half}} = -\ln\left(\frac{1}{2}\right) \frac{MR}{k_1 k_2} \approx 0.7 \frac{MR}{k_1 k_2}$$

Example

Suppose
$$k_1 = 7$$
, $\frac{MR}{k_2} = 20$,
 $V_B = 7s + 20 \frac{ds}{dt}$

If the robot starts at rest and $7\mathsf{V}$ are applied then steady state speed is

$$s = rac{V_B}{k_1} = 1 \mathrm{m \ sec^{-1}}$$

 $au_{rac{1}{2}} pprox 0.7 rac{MR}{k_1 k_2} = 0.7 rac{20}{7} = 2 \mathrm{sec}$

Time taken to cover half the gap between current and steady-state speed.

Identification of a control problem

If K = 5, and $s_{\infty} = 8$, and the system takes 14 seconds to reach s = 6 starting from s = 0. What is the process equation?

• Determine A and B in

$$Ks_{\infty} = Brac{ds}{dt} + As$$

• General solution of the equation:

$$\tau = \frac{B}{A} \qquad s_{\infty} = \frac{C}{A}$$

where
$$C = Ks_{\infty} = 40$$



Solution of the process equation (unit scale)

• Thus
$$A = \frac{C}{s_{\infty}} = K = 5$$
, $B = \tau A$
• How do we obtain τ ? (Hint $\tau = 7s$, i.e. $B = 35$)

Process model

$$V_B = k_1 s + rac{M}{k_2} R rac{ds}{dt}$$

Stationary behaviour (steady state)

$$s(t o \infty) = rac{V_B}{k_1}$$

Inverse model:

$$V_B = k_1 \, s_{\sf goal}$$

Solution provides forward model:

$$s(t) = s_0 e^{-\frac{MR}{k_1 k_2}(t-t_0)} + \frac{V_B}{k_1} \left(1 - e^{-\frac{MR}{k_1 k_2}(t-t_0)}\right)$$

- In order to derive a process model, we need to understand the physics of the system
- For simple processes, the system can be characterised by stationary state and the time constant of the approach towards this state
- Given the model equation, a few measurements can help to derive the explicit model equation and thus to obtain the trajectory of the system